# Measurement and Calculation of the $Ybl_2-AI$ (A=Na, K, Rb, Cs) Phase Diagrams<sup>1</sup>

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The phase diagrams of the Ybl<sub>2</sub>-AI (A=Na,K,Rb,Cs) systems have been measured by differential thermal analysis and X-ray powder diffraction. A set of thermodynamic functions have been optimized based on an interactive computer-assisted analysis. The optimized phase diagrams and thermodynamical data are self-consistent. © 1995 Academic Press, Inc.

## 1. INTRODUCTION

It has been reported that some compounds of rare earth and alkali halides (such as NaScI<sub>4</sub>, CsCeI<sub>4</sub>, CsNdI<sub>4</sub>, and CsLaI<sub>4</sub>) and the divalent samarium compounds NaSmI<sub>3</sub> and CsSmI<sub>3</sub> (1–6) show higher vapor pressures than those of the rare earth salts alone. This has been confirmed by the observation of an increase in vapor pressure over a molten mixture of cerium iodide and sodium iodide in high-intensity discharge lamps (5). It is believed that the complexes of rare earth and alkali halides would be potentially useful as new filling materials for discharge lamps. Therefore, it is very important to study the phase diagrams and thermodynamic properties of the systems containing rare earth and alkali halides.

A few phase diagrams for divalent rare earth (RE) halides and alkali (A) halides have been published (7-11). The compounds  $A \text{EuCl}_3$  (A = Cs, Rb).  $A \text{Eu}_2 \text{Cl}_5$  (A = Na, K, Rb, Cs, Tl), and  $K_2 \text{EuCl}_4$  have been reported in the  $\text{EuCl}_2$ -A Cl binary systems (8). In the  $\text{SmI}_2$ -A I systems (11), the compounds  $A \text{Sm}_2 \text{I}_5$  (A = K, Rb, Cs),  $A \text{SmI}_3$  (A = Rb, Cs),  $A_2 \text{SmI}_4$  (A = Rb, Cs), and  $A_3 \text{SmI}_5$  (A = Rb, Cs) have also been reported. To ascertain the general pattern of the phase relationships of binary  $R \text{EX}_2$ -A X

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systems and to search for new luminous materials for discharge lamps, the phase diagrams of  $Ybl_2-AI$  (A = Na, K, Rb, Cs) systems are experimentally determined and theoretically calculated in this paper.

#### 2. EXPERIMENTAL DETAILS

YbI<sub>2</sub> was prepared by reaction of ytterbium with  $HgI_2$  (12). High-purity commercial reagent grade NaI, KI, RbI, CsI (melting points 661, 680, 646 and 626°C, respectively) were used without further purification. However, they were dried by heating in vacuum (2.7 × 10<sup>-4</sup> Pa) at 350°C for 3 hr before use. The purities of SmI<sub>2</sub> and AI were checked by X-ray and thermal analyses.

YbI<sub>2</sub>-AI samples (13-15) with different molar ratios were prepared by weighing and mixing YbI<sub>2</sub> and AI in a dry box under an argon atmosphere in which the oxygen concentration was less than 0.5%. Water was removed by condensation with liquid nitrogen as well. Each sample was sealed in a quartz ampoule in vacuum (2.7 × 10<sup>-4</sup> Pa). To reach equilibrium, the YbI<sub>2</sub>-AI samples were heated at 400-500°C for 240 hr. Differential thermal curves of the samples were recorded with a differential thermal analyzer (homemade, model 4-1; heating rate, 5°C min<sup>-1</sup>; temperature accuracy,  $\pm 1\%$ ). A phase analysis was performed on the basis of X-ray power diffraction data, obtained with a 114.6- or 57.3-mm Debye-Scherrer Camera and nickel-filtered CuK $\alpha$  radiation ( $\lambda$  = 0.154178 nm).

### 3. EXPERIMENTAL RESULTS

The experimental results are shown in Figs. 1-4. The phase diagram of the YbI<sub>2</sub>-NaI system (Fig. 1) shows that

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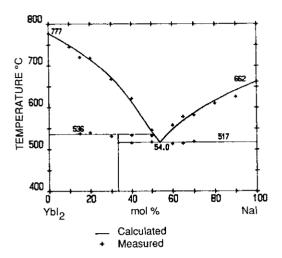


FIG. 1. YbI<sub>2</sub>-NaI phase diagram.

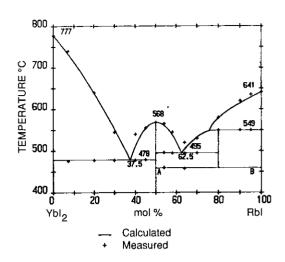


FIG. 3. Ybl2-Rbl phase diagram.

this system involves one incongruently melting compound NaYb<sub>2</sub>I<sub>5</sub> with a peritectic temperature of 536°C; the eutectic point is located at 54.0 mole% NaI and 517°C. In the YbI<sub>2</sub>–KI system (Fig. 2), there is also one incongruently melting compound KYbI<sub>3</sub>, which has the peritectic temperature 504°C, and a eutectic point located at 455°C, at 64.0 mole% KI.

The congruently melting compound  $RbYbI_3$ , with a melting temperature of  $568^{\circ}C$ , and the incongruently melting compound  $Rb_4YbI_6$ , with a peritectic temperature of  $549^{\circ}C$ , are presented in Fig. 3. There are also two eutectic points measured at 478 and  $495^{\circ}C$  at 37.5 and 62.5 mole% RbI in the  $YbI_2$ -RbI system.

Figure 4 shows that the melting point of the congruently melting compound CsYbI<sub>3</sub> is 670°C; the peritectic temperatures of the two incongruently melting compounds

Cs<sub>2</sub>YbI<sub>4</sub> and Cs<sub>6</sub>YbI<sub>8</sub> are 534 and 557°C, respectively. Also, two eutectic points are observed at 565 and 506°C at 32.0 and 76.0 mole% CsI.

In all four  $YbI_2$ -AI (A = Na, K, Rb, Cs) systems, the molar ratios at the eutectic points have been confirmed by the Tammann Trigon method, in which the endothermal curve determined by DTA is plotted against composition and the point of maximum deflection identifies the eutectic point.

The formation of the ternary ytterbium and alkali iodides, except Rb<sub>4</sub>YbI<sub>6</sub>, Cs<sub>2</sub>YbI<sub>4</sub>, and Cs<sub>6</sub>YbI<sub>8</sub> have been confirmed by X-ray diffraction measurements at room temperature. The failure to detect the three complexes by X-ray diffraction at room temperature may be due to the decomposition of this compound below 450°C. The existence of the three complexes should be

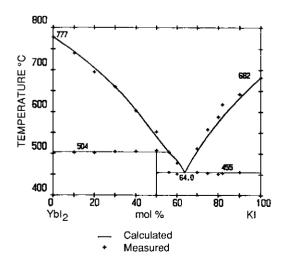


FIG. 2. YbI<sub>2</sub>-KI phase diagram.

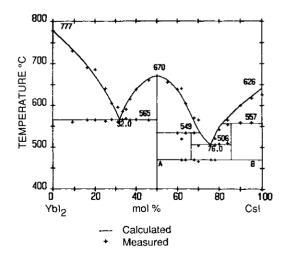


FIG. 4. Ybl<sub>2</sub>-CsI phase diagram.

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further confirmed by high-temperature X-ray measurements.

#### 4. OPTIMIZATION AND CALCULATION

### 4.1. Thermodynamic Model

For many charge-asymmetric molten salt systems  $(C_{\rm m}X_{\rm p}-D_{\rm n}X_{\rm r})$ , a better representation with fewer coefficients is obtained, if the excess thermodynamic properties of liquid solution is expressed in terms of the equivalent fraction, rather than of the mole fraction (16-18). The former is defined as

$$Z_{\rm A} = \frac{pX_{\rm A}}{pX_{\rm A} + rX_{\rm B}} \quad Z_{\rm B} = \frac{rX_{\rm B}}{pX_{\rm A} + rX_{\rm B}},$$
 [1]

where A and B stand for  $C_{\rm m}X_{\rm p}$  and  $D_{\rm n}X_{\rm r}$ , respectively, and  $X_{\rm A}$  and  $X_{\rm B}$  are mole fraction of A and B.

Obviously,  $Z_A/Z_B$  represents the charge number ratio of C and D ions. Therefore, the interaction between unit charges is considered. Then, the molar and excess molar Gibbs energy in liquid are expressed as

$$G_{\rm m}^{\rm l} = X_{\rm A} {}^{\rm o}G_{\rm A}^{\rm l} + X_{\rm B} {}^{\rm o}G_{\rm B}^{\rm l} + RT(X_{\rm A} \ln X_{\rm A} + X_{\rm B} \ln X_{\rm B}) + {}^{\rm E}G_{\rm m}^{\rm l}$$
[2]

$${}^{\mathrm{E}}G_{\mathrm{m}}^{\mathrm{I}} = (pX_{\mathrm{A}} + rX_{\mathrm{B}}) \sum_{\alpha} \sum_{\beta} (h_{\alpha\beta} - Ts_{\alpha\beta}) Z_{\mathrm{A}}^{\alpha} Z_{\mathrm{B}}^{\beta}, \qquad [3]$$

where  ${}^{o}G_{A}$  and  ${}^{o}G_{B}$  are the standard Gibbs energy of A and B in the liquid state;  $\alpha$  and  $\beta$  are positive integral powers; and  $h_{\alpha\beta}$  and  $s_{\alpha\beta}$  are assumed to be independent of T and related to enthalpy of mixing and excess entropy of mixing.

The partial excess Gibbs energy of i (i = A or B) in liquid ( ${}^{E}G$ ) can be obtained by differentiating Eq. [3] via

$${}^{\mathrm{E}}G_{\mathrm{i}}^{\mathrm{l}} = {}^{\mathrm{E}}G_{\mathrm{m}}^{\mathrm{l}} + (1 - X_{\mathrm{i}}) \frac{d {}^{\mathrm{E}}G_{\mathrm{m}}^{\mathrm{l}}}{dX_{\mathrm{i}}}$$
 [4]

to give

$${}^{\mathrm{E}}G_{\mathrm{A}}^{\mathrm{I}} = p \sum_{\alpha} \sum_{\beta} (h_{\alpha\beta} - Ts_{\alpha\beta}) \times [\alpha + (1 - \alpha - \beta)Z_{\mathrm{A}}] Z_{\mathrm{A}}^{\alpha-1} Z_{\mathrm{B}}^{\beta} \quad [5]$$

$${}^{\mathrm{E}}G_{\mathrm{B}}^{\mathrm{I}} = r \sum_{\alpha} \sum_{\beta} (h_{\alpha\beta} - Ts_{\alpha\beta}) \times [\beta + (1 - \alpha - \beta)Z_{\mathrm{B}}] Z_{\mathrm{A}}^{\alpha} Z_{\mathrm{B}}^{\beta-1}. \quad [6]$$

In the above formulas the coefficients  $h_{\alpha\beta}$  and  $s_{\alpha\beta}$  can be derived from a critical, self-consistent analysis of all the available diverse experimental thermodynamic and phase diagram data (19).

TABLE 1
Thermodynamic Properties of YbI<sub>2</sub> and AI

| Comp. | Tofus(K) | $A \times 10^{-3}$ | В        | C × 10 <sup>3</sup> | D       | E × 10 <sup>-5</sup> |
|-------|----------|--------------------|----------|---------------------|---------|----------------------|
| YbI,  | 1050     | 30.554             | - 29.099 | 0                   | 0       | 0                    |
| NaI   | 933      | 13.940             | 88.676   | 6.027               | -15.975 | 0                    |
| KI    | 954      | 4.656              | 211.211  | 14.460              | -33.547 | 2.46                 |
| кы    | 913      | 0.330              | 120.108  | 5.502               | -18.410 | 0                    |
| CsI   | 894      | 48.446             | -358.448 | -21.213             | 47.488  | 4.04                 |

# 4.2. Thermodynamic Data

The thermodynamic data of AI are selected from the literature (20); however, the thermodynamic data of YbI<sub>2</sub> have not been reported. To optimize and calculate the phase diagrams, the heat of fusion of YbI<sub>2</sub> is estimated from the YbI<sub>2</sub>-AI phase diagrams. It is known (21, 22) that for a melting transition, for example, as the composition approaches a pure component i, the difference between the slopes of the liquidus and solidus curves,  $dX_i^l/dT$  and  $dX_i^s/dT$ , is thermodynamically determined by the enthapy of fusion,  $\Delta H_{\Omega}^o$  and melting point,  $T_{\Omega}$ . That is,

$$\lim_{x_i \to 1} \left( \frac{dX_i^1}{dT} - \frac{dX_i^s}{dT} \right) = \frac{\Delta H_{f(i)}^o}{\nu R T_{f(i)}^2},$$
 [7]

where R is the gas constant and  $\nu$  is the number of "foreign particles" which are not present in the solvent originally, but introduced by the addition of one "molecule" of solute at infinite dilution. Equation [7] is independent of any model and can be used for estimating the enthalpy of fusion of pure component i. For YbI<sub>2</sub>-AI systems,  $\nu = 1$ ,  $\lim_{x_{r\to 1}} (dX_i^s/dT) = 0$ . Therefore,  $\Delta H_{f(YbI_2)}^s$  can be calculated to be 30,554 J mole<sup>-1</sup> from Eq. [7].

With the aid of all these data, Gibbs energies of fusion of various iodides are given by

$$\Delta G_{\rm f}^{\rm o} = {\rm A} + {\rm B}T + {\rm C}T^2 + {\rm D}T \ln T + {\rm E}/T {\rm J} \,{\rm mole}^{-1},$$
 [8]

where the values of the coefficients are listed in Table 1.

# 4.3. Calculation and Discussion

For the systems of  $YbI_2(A)-AI(B)$ , there is no solid solubility, so the excess partial Gibbs energies of A can be calculated at points along their respective liquidus lines from the well-known expression

$$RT \ln(1 - X_{\rm B}) + {}^{\rm E}G_{\rm A}^{\rm I} = -\Delta G_{\rm f(A)}^{\rm o}.$$
 [9]

Analogously for B, one obtains

TABLE 2
Excess Enthalpies and Entropies of the YbI<sub>2</sub>-AI Systems

| System                | $h_{11} \times 10^{-3}$ | $h_{12}\times 10^{-3}$ | s <sub>11</sub> | s <sub>12</sub> |
|-----------------------|-------------------------|------------------------|-----------------|-----------------|
| YbI <sub>2</sub> -NaI | -31.023                 | 51.223                 | -30.557         | 50.904          |
| Ybl <sub>2</sub> -KI  | -9.347                  | -15.236                | -0.751          | -19.365         |
| YbI <sub>2</sub> -RbI | 79.436                  | -9.819                 | 151.826         | -61.379         |
| YbI <sub>2</sub> -CsI | -32.819                 | -17.893                | 1.407           | -48.423         |

$$RT \ln X_{\rm B} + {}^{\rm E}G_{\rm B}^{\rm l} = -\Delta G_{\rm f(B)}^{\rm o}.$$
 [10]

In general, for any constituent  $A_m B_n$ 

$$mRT \ln (1 - X_B) + nRT \ln X_B + m^E G_A^I + n^E G_B^I$$
  
=  $-\Delta G_{f(A_m B_n)}^o$ . [11]

At each experimental liquidus temperature and composition,  ${}^{E}G_{A}^{I}$  and  ${}^{E}G_{B}^{I}$  can be calculated vis Eqs. [9] and [10]. Then, all coefficients  $h_{\alpha\beta}$  and  $s_{\alpha\beta}$  can be derived simultaneously via Eqs. [5] and [6] using the program FITBIN (18). The optimized equations

$$H_m^{M} = (pX_A + rX_B)(h_{11}Z_AZ_B + h_{12}Z_AZ_B^2) \text{ J mole}^{-1}$$
 [12]  

$${}^{E}S_m = (pX_A + rX_B)(s_{11}Z_AZ_B + s_{12}Z_AZ_B^2)$$

$$\text{J mole}^{-1} \text{ K}^{-1}$$
 [13]

are obtained, where the coefficients  $h_{11}$ ,  $h_{12}$ ,  $s_{11}$ , and  $s_{12}$  are listed in Table 2.

Assuming that Eqs. [12] and [13] interpolate well across the central composition region between the YbI<sub>2</sub>- and AI-liquidus lines, one can then use Eq. [11] to calculate the Gibbs energies of fusion of the ternary ytterbium and alkali iodides. The resultant expressions for the Gibbs energies of fusion are obtained as

TABLE 3
Thermodynamic Properties of Intermediate Compounds

|                                  |   | $\Delta G_{\rm f}^{\rm o} = a + bT$ (J/mole) |          |  |
|----------------------------------|---|--|----------|--|
| Int. Comp.                       | $T^{\diamond}_{\mathrm{fus}}(\mathbf{K})$ | $a \times 10^{-3}$                           | b        |  |
| NaYb <sub>2</sub> I <sub>5</sub> | 809ª                                      | 11.456                                       | - 13.318 |  |
| KYbI,                            | 777ª                                      | 6.745  | -8.576   |  |
| $RbYbI_3$                        | 841                                       | 8.615  | -10.238  |  |
| Rb <sub>4</sub> YbI <sub>6</sub> | 822ª                                      | 18.996                                       | -23.036  |  |
| CsYbI <sub>3</sub>               | 943                                       | 16.021                                       | - 16.994 |  |
| $Cs_2YbI_4$                      | 807ª                                      | 10.815                                       | -13.278  |  |
| Cs <sub>6</sub> YbI <sub>8</sub> | 830ª                                      | 6.885  | -8.199   |  |

<sup>&</sup>lt;sup>a</sup> Peritectic temperature.

$$\Delta G_{f(A_-B_-)}^{o} = a + bT J \text{ mole}^{-1}, \qquad [14]$$

where the coefficients a and b are listed in Table 3. The measured melting points or peritectic temperatures are presented in Table 3.

According to the thermodynamic data optimized above, the phase diagrams of YbI<sub>2</sub>-AI binary systems were calculated by using the program POTCOMP (18) as shown in Figs. 1-4, in which "+" denotes the experimental data. It is clear that the calculated lines agree well with the experimental data.

Comparing the four YbI<sub>2</sub>-AI phase diagrams, we observe that the larger the ionic radius of the alkali is, the larger the number is and the greater the stability of compounds contained in the system is. This observation is consistent with those of the SmI<sub>2</sub>-AI (A = Na, K, Rb, Cs) (11) and  $AEF_2$ -AF (AE, alkaline earth metal; A, alkali metal) (10) systems.

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